

- Mucool - Linac area development - Relief valve calculations

HYDRONGEN RELIEF VALVE SIZING FOR THE MUCOOL LH2 ABSORBER

Relief Valve for the main hydrogen abs (6.87 liter)

Calculation of the relief flow capacity

CGA S-1.3-1995 sizing of the primary relief valve as per paragraph 5.2.2

Vessel MAWP (psig)	17.630 (P)
Flow rating pressure (psia)	39.119 P
vi, specific volume of liquid relieved (ft ³ /lb)	0.243 V
C: cst of gas of vapor related to ratio of specific heat	357.000 C
Z: compressibility factor a the temperature T and flow rating pressure P	1.000 Z
M: molar weight of fluid	2.020 M
Temperature at maximum flow rate (R)	44.820

Relief valve flow capacity in SCFM of air - loss of insulation vacuum

3.217E-04

CGA p10

6.8 l=0.24 ft³

$$Q_a = \frac{0.0085 * P V}{C} \sqrt{\frac{M}{Z}}$$

F (correction factor for heat transfer)

1.000 F

Gu, gaz factor for ininsulated container

45.800 Gu

Mean of absorber surface area (in+out) (square feet)

1.978 A

Relief valve flow capacity in SCFM of air - fire case

80.13

$$Q = A F * G * u A^{0.8}$$

V (SCFM)

80.126

M (hydrogen)

2.020

W, flow capacity (lbs/hr)

25.6

$$W = \frac{M * V}{6.3}$$

Calculation of the relief valve area

W (lbs/hr.)	25.610
V (SCFM)	80.126
M (hydrogen)	2.020
Temperature at maximum flow rate (R)	44.820
Z (-)	1
C (hydrogen)	357.000
Kd, coeff. of discharge	0.9575
Kb, capacity corrector factor	1
P1, upstream relief pressure (psia)	39.1

Area, of the relief valve (in²)

0.353

$$A = \frac{W \sqrt{T Z}}{C K_b K_d P_1 \sqrt{M}}$$

Area, of the relief valve (in²)

9.021E-03

$$A = \frac{V \sqrt{M T Z}}{6.3 C K_d K_b P_1}$$

Comparison with the absorber nozzle geometry

dh2ct (in)

0.750

The cooling tube area is (in²)

0.442

C/C for the worst case scenario (fire) the section of the current nozzle will be enough to evacuate the hydrogen flow